

**Division Information**

Engineer:	Stephanie Chaousy, PE
Control Engineer:	Chris Laplante
Review Date:	11/05/2014
Application Date:	06/27/2014

**Attainment Status**

PM10	Attainment
PM2.5	Attainment
SOx	Attainment
NOx	Attainment
VOC	Attainment
CO	Attainment

**Facility Information**

Permit No.		14L1168	
AIRs	County #	073	Lincoln
	Facility #	0085	
	Point #	014	
Facility Equipment ID			
Company Name:		Wiepking-Fullerton LLC	
Source Name:		Aloha Mula Gas Plant	
Source Location:		SESW Section 19, T10S, R55W	
SIC:		1311	
Elevation (feet):		5250	
X	New Permit (CP1)	Modification (Issuance #)	APEN Required/Permit Exempt
		Transfer of Ownership	APEN Exempt/Permit Exempt
Notes			

**Equipment Description**

This source vents natural gas from:	a well head separator
Emissions from this source are:	routed to an enclosed flare

Natural gas venting from a well head separator. Emissions from this source are routed to an enclosed flare.

Emission Calculation Method

EPA Emission Inventory Improvement Program Publication: Volume II, Chapter 10 - Displacement Equation (10.4-3)

$$Ex = Q * MW * Xx / C$$

Ex = emissions of pollutant x

Q = Volumetric flow rate/volume of gas processed

MW = Molecular weight of gas = SG of gas \* MW of air

Xx = mass fraction of x in gas

C = molar volume of ideal gas (379 scf/lb-mol) at 60F and 1 atm

Throughput (Q)	42 MMscf/yr	4794.5 scf/hr	3.57 MMscf/mo
MW	25.740 lb/lb-mol	0.001 MMscf/d	

	mole %	MW	lbx/lbmol	mass fraction	E	lb/hr	lb/yr	tpy
Helium	0.34	4.0026	0.014	0.001	Helium	0.2	1508	0.75
CO2	0.43	44.01	0.189	0.007	CO2	2.4	20972	10.49
N2	20.94	28.013	5.866	0.228	N2	74.2	650049	325.02
methane	48.4396	16.041	7.770	0.302	methane	98.3	861077	430.54
ethane	13.8556	30.063	4.165	0.162	ethane	52.7	461602	230.80
propane	11.5386	44.092	5.0876	0.198	propane	64.4	563797	281.90
isobutane	1.2252	58.118	0.7121	0.028	isobutane	9.0	78909	39.45
n-butane	2.541	58.118	1.4768	0.057	n-butane	18.7	163654	81.83
isopentane	0.3011	72.114	0.2171	0.008	isopentane	2.7	24062	12.03
n-pentane	0.233	72.114	0.1680	0.007	n-pentane	2.1	18620	9.31
cyclopentane	0.0145	70.13	0.0102	0.000	cyclopentane	0.1	1127	0.56
n-Hexane	0.0117	86.18	0.0101	0.000	n-Hexane	0.1	1117	0.56
cyclohexane	0.0030	84.16	0.0025	0.000	cyclohexane	0.0	280	0.14
Other hexanes	0.0422	86.18	0.0364	0.001	Other hexanes	0.5	4030	2.02
heptanes	0.0046	100.21	0.0046	0.000	heptanes	0.1	511	0.26
methylcyclohexane	0.0007	98.19	0.0007	0.000	methylcyclohexane	0.0	76	0.04
224-TMP	0	114.23	0.0000	0.000	224-TMP	0.0	0	0.00
Benzene	0.0076	78.12	0.0059	0.000	Benzene	0.1	658	0.33
Toluene	0.0008	92.15	0.0007	0.000	Toluene	0.0	82	0.04
Ethylbenzene	0	106.17	0.0000	0.000	Ethylbenzene	0.0	0	0.00
Xylenes	0	106.17	0.0000	0.000	Xylenes	0.0	0	0.00
C8+ Heavies	0.0003	968.071	0.0029	0.000	C8+ Heavies	0.0	322	0.16
VOC mass fraction:				0.3005	Total VOC Emissions (Uncontrolled)		428.6	
				25.740	annual limit assuming 95% control		21.4	
					monthly limit assuming 95% control (lb/mo.)		3640.4	

Notes

Mole %, MW, and mass fractions from Critter Creek 2-03H gas analysis.  
Emissions are based on 8760 hours of operation per year.  
I calculated the average MW of C8+ based on the average MW on the analysis for the gas.

**Flaring Information**

Equipment Description

Flare to combust produced gas until pipeline is available at this wellhead facility.

Manufacturer	Leed	
Model	L-30-007-000	
Serial Number		
Gas Heating Value	1068	Btu/scf
Throughput	44856	MMBtu/yr

Combustion emission factor source: [AP-42: Chapter 13.5](#)

0.068	lb NOX/MMBtu	0.37	lb CO/MMBtu
1.53	tpy NOX	8.30	tpy CO

**Emissions Summary**

Uncontrolled/PTE	1.53	tpy NOX
	8.30	tpy CO
Controlled	428.623	tpy VOC
	21.431	tpy VOC

	Uncontrolled Total (lb/yr)	Bin	Scenario A Reportable?	Controlled Total (lb/yr)
Benzene	658	A	Yes	33
Toluene	82	C	No	4
Ethylbenzene	0	C	No	0
Xylenes	0	C	No	0
n-hexane	1117	C	Yes	56
224-TMP	0	C	No	0

**Regulatory Applicability**

**AQCC Regulation 1**

This source is subject to the opacity requirements for flares in Section II.A.5: 'No owner or operator of a smokeless flare or other flare for the combustion of waste gases shall allow or cause emissions into the atmosphere of any air pollutant which is in excess of 30% opacity.'

**AQCC Regulation 2**

Section I.A applies to all emission sources. "No person, wherever located, shall cause or allow the emission of odorous air contaminants from any single source such as to result in detectable odors which are measured in excess of the following limits: For areas used predominantly for residential or commercial purposes it is a violation if odors are detected after the odorous air has been diluted with seven (7) or more volumes of odor free air."

**AQCC Regulation 3**

Part A:	An APEN is required for this source because uncontrolled VOC emissions exceed two tons per year in an attainment area.
Part B:	A permit is required for this source because uncontrolled VOC emissions from this facility exceed five tons per year in an attainment area. This source is not subject to Section III.D.2 (Minor Source RACT) because it is not located in a nonattainment area.
Is public comment required?	Public Comment Required

**Facility Status**

This facility is a synthetic minor of VOC for Title V applicability.  
This facility is a synthetic minor source of VOC for PSD applicability.

**Division Information**

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Application Date:	06/27/2014

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PM10	Attainment
PM2.5	Attainment
SOx	Attainment
NOx	Attainment
VOC	Attainment
CO	Attainment

**Facility Information**

Permit No.		14L1178	
AIRs	County #	073	Lincoln
	Facility #	0099	
	Point #	003	
Facility Equipment ID			
Company Name:		Wiepking-Fullerton LLC	
Source Name:		Kauai #2	
Source Location:		SWNE Section 6, T10S, R55W	
SIC:		211111	
Elevation (feet):		5262	
X	New Permit (CP1)	Modification (Issuance #)	APEN Required/Permit Exempt
		Transfer of Ownership	APEN Exempt/Permit Exempt
Notes			

**Equipment Description**

This source vents natural gas from:	a well head separator
Emissions from this source are:	routed to an enclosed flare

Natural gas venting from a well head separator. Emissions from this source are routed to an enclosed flare.

Emission Calculation Method

EPA Emission Inventory Improvement Program Publication: Volume II, Chapter 10 - Displacement Equation (10.4-3)

$$Ex = Q * MW * Xx / C$$

Ex = emissions of pollutant x

Q = Volumetric flow rate/volume of gas processed

MW = Molecular weight of gas = SG of gas \* MW of air

Xx = mass fraction of x in gas

C = molar volume of ideal gas (379 scf/lb-mol) at 60F and 1 atm

Throughput (Q)	15 MMscf/yr	1712.3 scf/hr	1.27 MMscf/mo
MW	25.740 lb/lb-mol	0.000 MMscf/d	

	mole %	MW	lbx/lbmol	mass fraction	E	lb/hr	lb/yr	tpy
Helium	0.4105	4.0026	0.016	0.001	Helium	0.1	650	0.33
CO2	0.43	44.01	0.189	0.007	CO2	0.9	7490	3.74
N2	20.94	28.013	5.866	0.228	N2	26.5	232161	116.08
methane	48.4396	16.041	7.770	0.302	methane	35.1	307528	153.76
ethane	13.8556	30.063	4.165	0.162	ethane	18.8	164858	82.43
propane	11.5386	44.092	5.0876	0.198	propane	23.0	201356	100.68
isobutane	1.2252	58.118	0.7121	0.028	isobutane	3.2	28182	14.09
n-butane	2.541	58.118	1.4768	0.057	n-butane	6.7	58448	29.22
isopentane	0.3011	72.114	0.2171	0.008	isopentane	1.0	8594	4.30
n-pentane	0.2475	72.114	0.1785	0.007	n-pentane	0.8	7064	3.53
cyclopentane	0	70.13	0.0000	0.000	cyclopentane	0.0	0	0.00
n-Hexane	0.0117	86.18	0.0101	0.000	n-Hexane	0.0	399	0.20
cyclohexane	0.0000	84.16	0.0000	0.000	cyclohexane	0.0	0	0.00
Other hexanes	0.0452	86.18	0.0390	0.002	Other hexanes	0.2	1542	0.77
heptanes	0.0053	100.21	0.0053	0.000	heptanes	0.0	210	0.11
methylcyclohexane	0	98.19	0.0000	0.000	methylcyclohexane	0.0	0	0.00
224-TMP	0	114.23	0.0000	0.000	224-TMP	0.0	0	0.00
Benzene	0.0076	78.12	0.0059	0.000	Benzene	0.0	235	0.12
Toluene	0.0008	92.15	0.0007	0.000	Toluene	0.0	29	0.01
Ethylbenzene	0	106.17	0.0000	0.000	Ethylbenzene	0.0	0	0.00
Xylenes	0	106.17	0.0000	0.000	Xylenes	0.0	0	0.00
C8+ Heavies	0.0003	-93.346	-0.0003	0.000	C8+ Heavies	0.0	-11	-0.01

VOC mass fraction: 0.3004  
25.740

Total VOC Emissions (Uncontrolled) 153.0  
annual limit assuming 95% control 7.7  
monthly limit assuming 95% control (lb/mo.) 1299.7

Notes

Mole %, MW, and mass fractions from Aloha Mula Gas Plant (4/11/2013) gas analysis.  
Emissions are based on 8760 hours of operation per year.  
I calculated the average MW of C8+ based on the average MW on the analysis for the gas.

**Flaring Information**

Equipment Description

Flare to combust produced gas until pipeline is available at this wellhead facility.

Manufacturer	Leed	
Model	TBD	
Serial Number	TBD	
Gas Heating Value	1068	Btu/scf
Throughput	16020	MMBtu/yr

Combustion emission factor source: AP-42: Chapter 13.5

0.068 lb NOX/MMBtu	0.37 lb CO/MMBtu
0.54 tpy NOX	2.96 tpy CO

**Emissions Summary**

			Operator
Uncontrolled/PTE	0.54	tpy NOX	0.53
	2.96	tpy CO	2.88
Controlled	153.024	tpy VOC	148.78
	7.651	tpy VOC	7.4

\*I believe the difference in calculations is a rounding issue. I will permit operator's calculations

	Uncontrolled Total (lb/yr)	Operator uncontrolled	Scenario A Reportable?	Controlled Total (lb/yr)	Operator controlled
Benzene	235	228	Yes	12	11
Toluene	29	28	No	1	1
Ethylbenzene	0	-	No	0	-
Xylenes	0	-	No	0	-
n-hexane	399	388	No	20	19
224-TMP	0	-	No	0	-

**Regulatory Applicability**

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